

Tank Inspector(s) J. Martin (STI #AC 32455) and M. Emert

Name Plate/Construction

Circumference: 37.75'

Steel Stainless Steel Plastic Aluminum Fiberglass

Build Date 2000 Manufacturer Palmer Manufacturing and Tank

Build Std: API-650 API-12C API-12F UL-142 Re-Erected Unknown

Date Last External _____ Date Last Internal _____

Name Plate Data

Dia/Width: 12.00 ft Must be <=30 ft

Height: 42.00 ft Must be <=50 ft

Length: _____ ft

Capacity: 35,291 GAL

STI Not applicable for tanks over 50,000 Gal.

Product Service Basestock

Specific Gravity 1.00

Ambient Heated

Refrigerated

Operating Temperature 170 F

STI Not applicable for heated tanks over 200°F



Tank Description

Vertical Horizontal Box Tote Other _____

Foundation: Grade Ringwall Concrete Pad Saddles Skids Other

Bottom: Welded Riveted Bolted N/A Year Installed: _____

No Coating Thin Coating Thick Coating

Pan Type Cathodic Protection Double Bottom Leak Detection

Shell: Welded Riveted Bolted Combination

Lap welded Insulated Double Wall Containment Vessel

Horizontal Tank Heads: Flat Hemispherical Dish

Roof: Cone Flat Geo-Dome Dome Open/None N/A

Roof Access: Spiral Stair Radial Stair Catwalk Ladder None

1. Spill Control

None

- Containment AST Dbl Wall/Bottom Dike Area Remote Impound in Building

2. CRDM (Continuous Release Detection Method)

None

RPB (Release Prevention Barrier)

Type Concrete Pad Liner Steel Plate Other _____

Double Wall/Bottom with Interstitial Space

OK Not OK Not Checked

Elevated

3. AST Category

Category 1

- 1 Any Tank with Both Spill Control and CRDM
 - 2 Single wall AST in contact with ground NO CRDM Has Spill Control
 - 3 Single wall AST in contact with ground has CRDM NO Spill Control
- Vertical AST on concrete pad CRDM has NO Spill Control
Single/Double wall AST Has CRDM NO Overfill Protection

4. Venting

- Open vents not elevated 12 feet Open vents not vented outside building
 Uses long bolted Manway as emergency vent Vapor recovery system

Primary Vent Open Pressure/Vacuum Pressure Size: 8.00"

Secondary Vent Open Pressure/Vacuum Pressure Size: _____

Emergency Vent Open Pressure/Vacuum Pressure Size: _____

Interstice Vent Open Pressure/Vacuum Pressure Size: _____

5. Comments

The tank was located inside a building. The open vent was not vented outside the building.

The tank had an 8-inch open vent.

1. Foundation **Concrete Pad**

Anchorage: No Anchors Cable Tie Downs Anchor Bolts
Number of Anchors: 4 Size of Bolt (in) 1.00 Height (in) 14.00
Thickness of top plate (In) 0.526 Thickness of side plate (In) 0.520

Ringwall/Pad Dimensions: Distance from Bottom extension to edge (in) 5.00 Min 6.00 Max
Distance from top surface to grade (in) 23.00 Min 26.00 Max

Support Dimensions: Number of supports: Space between Supports (in)
Size of supports (in): Height of supports (in):
 No Pad Plate Pad Plate Stitch welded pad plate Seal welded pad plate

2. Undesirable Foundation Conditions

- Grade against tank Washout Voids under tank Hairline Cracks in concrete
- Large Cracks in concrete (>1/8") Exposed rebar Discontinuous Ringwall
- Corrosion of supports Anchor Bolt Corrosion Bottom extension corrosion

3. Undesirable Area Conditions

- Obvious settlement Water Against tank Drainage toward tank Excessive debris
- Vegetation by tank Moss under bottom No Containment Dike/Wall
- Damaged Containment Dike/Wall Product residue Wet Product by Tank

4. Comments

The tank was located inside a building.

1. External Tank Shell

Welded

- Seams Covered Rivets Unsealed Rivets Sealed Rivets Welded
- No Pad Plates Under Shell Brackets No Ice shields on All Item <2" Foam System

2. Coating Conditions

Like New Good Fair Poor No Coating

- Peeling Cracking Thinning Rust Stained Primer Only Areas not Coated

Insulation Conditions

Like New Good Fair Poor

- Sprayed Corrugated/ Banded Smooth Metal Areas Removed
- Tears Damaged Holes Penetrations Not Sealed Wet under Insulation

3. Undesirable Shell Conditions

- Weld Seam Corrosion Weld Pinholes Arc Strikes Weld Porosity Weld Slag
 - Weld Cracks Weld Undercut Lack of Fusion Holes in Shell Gouges in Shell
 - Inactive Corrosion Active Corrosion Surface Corrosion Corrosion Damage
- Deepest Shell Corrosion Found: __ Height above Grade __ Needs Evaluation

4. Shell Distortion and Buckling

- Peaking Banding Lower Shell Distortion Upper Shell Distortion Torn Plate
- Distortion around Nozzles/Repairs Minor Buckles Major Buckles Sharp Creases

5. Possible Improper Construction Practices

List Items Below

- Square Corner Inserts/Pads Lap Patches Unreinforced Penetration Split Repad
- No Telltale Hole in Repad Plugged Telltale Hole in Repad Improper Weld Space
- Insufficient Reinforcement Undersize Insert Cover Plate Thin Flange Thin

The repads of Shell Items C, L, and M did not have telltale holes.

The weld spacing of Shell Items C and G did not meet API standards.

Shell Items A, H, I, and J were over 2 inches in diameter and did not have repads.

6. Ground cables

Quantity 1

- None Found Not Attached Broken Improper Attachment

7. Level Gauge Manufacturer DP Harp Product Height: FT

- Float with Gauge Target Board Electronic Floats, Cables Guides not Attached
- Not Working Conduit damaged Needs Service

8. Top Angle Wind Girder

- None Toe In Toe Out Corrosion TA Weld Size Greater than 3/16"
- Damaged Welds Buckled Coating Failure Holds Water Buckled

Top Angle: Vertical (in) 2.50 Horizontal (in) 2.50 Thickness (in) 0.262

Wind girder: Vertical (in) Horizontal (in) Thickness (in)

Distance from Top of Tank (in):

9. Shell Vents and Overflows

- None Indicator Holes Screens Missing/Damaged Over Stairway Geo Dome

Number of Vents: Size (in): Distance from roof (in):

Number of Overflows: Size (in): Distance from roof (in):

10. Comments

The coating on the external shell and appurtenances was in good condition.

1. Internal Tank Shell **Welded**

- Product Build-Up Product Residue Lower Shell Coated Entire Shell Coated
- Shell Not Inspected Shell Welds Not Inspected

2. Undesirable Shell Conditions

- Weld Seam Corrosion Weld Pinholes Weld Porosity Weld Slag Weld Cracks
 - Weld Undercut Lack of Fusion Arc Strikes Holes in Shell Gouges in Shell
 - Weld Burrs Minor Shell Corrosion Shell Corrosion Damage
- Deepest Shell Corrosion Found: __ Height above Bottom __ Needs Evaluation

5. Possible Improper Construction Practices List Items Below

- Lap Patches Item Penetrates but Not Welded Hot Tap Drilled Hole for Coupling
 - No Pads on Gauge Pole Supports No Pads on Datum Plate Supports Undercut
 - Incomplete Shell Weld Lack-of-Fusion Cracked Weld Welds Not Visible
-
-

5. Internal Piping and Supports

- No Pads on Pipe Supports Pipe Support Welded to Both Pipe and Bottom
 - Inadequate Pipe Supports Corrosion on Piping Broken Welds No Diffuser
 - No Suction Trough Center Suction / Fill Has Floating Suction Line
-

6. Comments

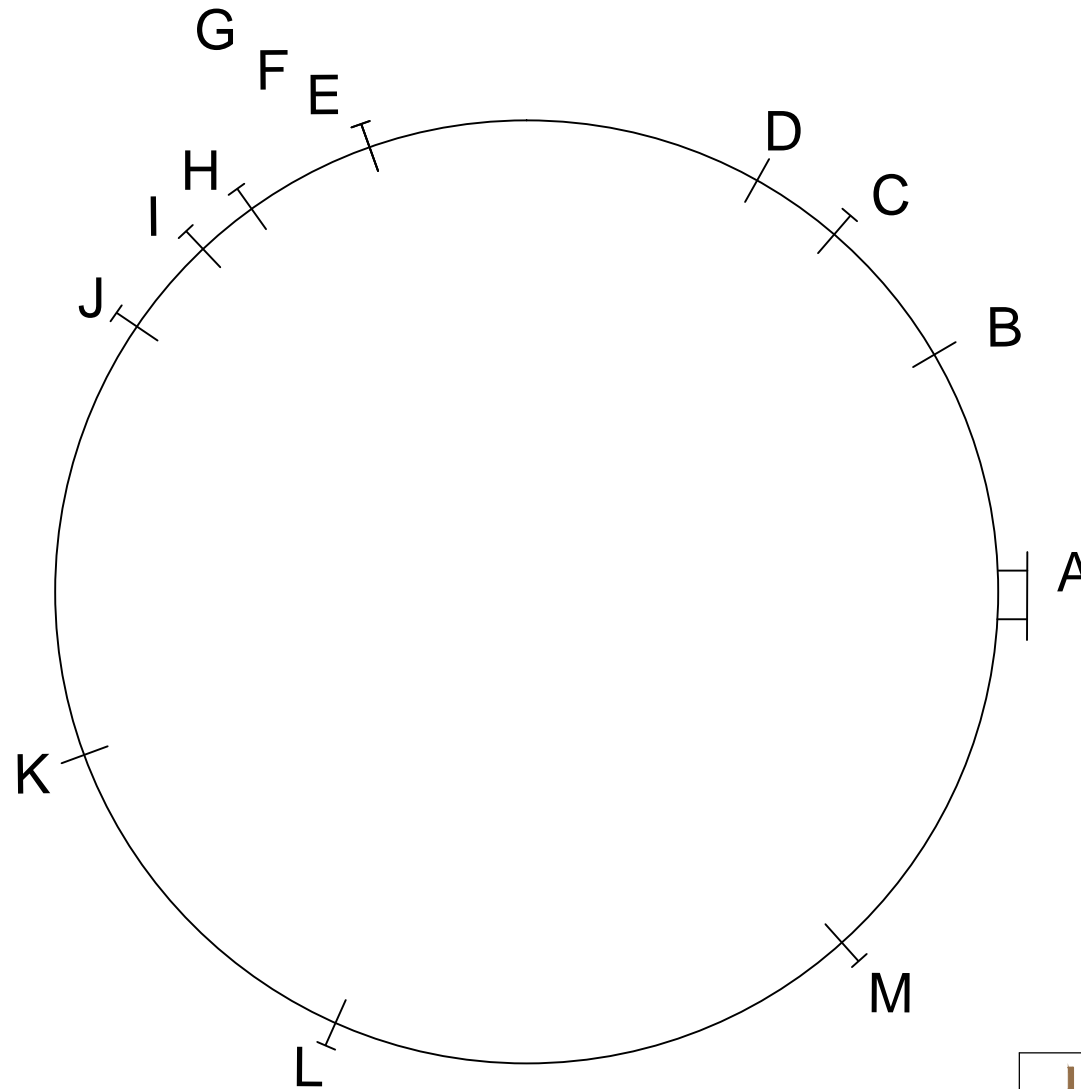
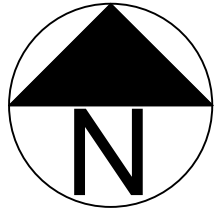
There was product residue on the internal shell.



Height is measured from bottom to the centerline of the item. Weld spaces are measured toe-to-toe of the welds.

ID	Size	TT hole	Shape*	Description	Location	Height	Repad/Insert			Neck Thicknesses				Weld Space	To**
							Width	Height	t	Top	Bottom	Left	Right		
A	24.00			Manway	0.00	30.00				0.399				16.50	CW
B	0.75			Coupling	3.20	30.00								28.00	CW
C	2.00		A	Nozzle	5.20	6.00	10.00	10.00	0.243	0.216				1.50	CW
D	0.75			Coupling	6.40	24.00								23.00	CW
E	3.00			Nozzle	11.50	Ring 7									
F	0.75			Coupling	11.50	24.00								12.00	G
G	4.00	1	C	Nozzle	11.50	6.00	10.00	10.00	0.247					0.00	CW
H	4.00			Nozzle	13.20	32.00				0.241				28.75	CW
I	4.00			Nozzle	14.00	20.00				0.242				17.00	CW
J	4.00			Nozzle	15.30	8.00				0.232				5.25	CW
K				Catwalk	21.00										
L	8.00		A	Nozzle w/ Mixer	25.80	36.00	26.00	26.00	0.249	0.293				23.75	CW
M	2.00		A	Nozzle	32.70	9.00	10.00	10.00	0.249	0.216				3.50	CW
N															
O															
P															
Q															
R															
S															
T															
U															
V															
W															
X															
Y															
Z															
AA															
BB															

** TS=Tombstone or low type repad, CW=Cornerweld, HW= Horz. weld, VW=Vertical Weld, R#=Repad of Item #, #=-Weld of Item#, PB=Pan Bottom weld



- | Couplings/Other
- ┆ Nozzles
- ┆┆ Manway
- Ladder
- Catwalk/Platform
- ┆ Stairs

		Job No:	652131	
		Tank Num:	DVOP 11	
		Date:	07-14-2021	
Customer:	AGP			
Location:	Hastings, NE			
	Diameter:	12.00	Height:	42.00
	Drawn by:	A Frye	Rev:	

STI-INTERNAL



Company: AGP
 Location: Hastings, NE

Job ID: 652131
 Date: 7/14/2021
 Tank: DVOP 11

Course	Height (in)	Shell Material	Joint Type*	Shell Thicknesses (in)		
				Bottom	Middle	Top
1	69.00		BW	0.250	0.246	0.246
				0.250	0.250	0.249
				0.249	0.248	0.250
				0.250	0.249	0.244
2	69.00		BW	0.248	0.247	0.247
3	68.75		BW	0.247	0.247	0.247
4	68.75		BW	0.250	0.250	0.251
5	68.75		BW	0.248	0.246	0.246
6	69.00		BW	0.248	0.249	0.244
7	68.50		BW	0.250	0.248	0.248
8						
9						
10						

* Joint Type: BW= Butt Weld, LW= Lap Weld, LR# = Lap Riveted (num of rivets), BR= Riveted Butt joint (Num Rivets on one side), BLT=Bolted

Total Height

Minimum Thickness written in Blue Font

Enter Vertical seam Location in CCW order from Start point.

1	36.30	11		21		31
2		12		22		32
3		13		23		33
4		14		24		34
5		15		25		35
6		16		26		36
7		17		27		37
8		18		28		38
9		19		29		39
10		20		30		40

Second Course offset _____

Third Course offset _____

1. Tank Roof

Cone

- No Access Limited Access Access Not Safe No Safety Tie Off
Slope, Run 24 inches Rise (in): 3.00

2. Coating Conditions

Like New Good Fair Poor No Coating

- Peeling Cracking Thinning Primer Only Areas Not Coated

Insulation Conditions

Like New Good Fair Poor

- Sprayed Corrugated/ Banded Smooth Metal Areas Removed
 Tears Damaged Holes Penetrations Not Sealed Wet under Insulation

3. Undesirable Roof Conditions

- Weld Seam Corrosion Weld Pinholes Weld Cracks Holes in Roof
 Inactive Corrosion Active Corrosion Surface Corrosion Corrosion Damage
 No Safety Bars on >30" Openings Thinnest RWT Found: 0.248" Needs Evaluation

4. Roof Distortion and Buckling

- Excessive Waviness Areas Holding Water Settlement of Support Structure
 Torn Plates Sharp Creases Roof Joint Not Frangible (3/16")

5. Vents and settings

List vent sizes and settings below

- Open Vents Pressure/Vacuum Vents Peripheral Vents Flame Arrestor
 Missing/Damaged Screens Vents Need Service Less than 8" Center Vent with IFR
The tank had an 8-inch open vent. The open vent extended to the lower level of the tank.

The open vent was not vented outside the building.

6. Comments

The coating on the external roof and appurtenances was in good condition.

1. Internal Tank Roof

Structurally Supported Self Supporting (No Structure)

Record column radius location and number of columns

Center	Bay 1	Bay 2	Bay 3	Bay 4
Radius 0				
Number 0				

2. Column Type, Size and Conditions

Structural Steel Steel Pipe Both Types

Dimensions (in)	Center Column	Outer Columns
Size of Members		

- Welded Riveted Bolted Bowed Twisted Out-of-Plumb Damaged
 Corroded Broken Welds No Drain Hole in Pipe

3. Column Base Type, Size and Conditions

H-Shaped T-Shaped Flat Plate

Dimensions (in)	Center Base	Outer Bases
Size of Members		
Bearing Plate		

- Welded Riveted Bolted Damaged Welded to Bottom No Guide Clips
 Insufficient Guide Clips Corroded No Bearing Plate Not Seal Welded

4. Rafter Conditions

- Bowed Twisted Hanging Sagging Corroded Damaged Not Radial

5. Roof Conditions

- Hole Corroded Un-Capped Opening Entire Underside Coated

6. Comments

Roof Nozzles and Appurtenances (Measure one and give quantity for peripheral vents)

	Type	Size	Radius*	Comment
A	Nozzle	8.00 "	0.00'	
B	Nozzle	6.00 "	5.00'	
C	Coupling	2.00 "	5.00'	
D	Nozzle	6.00 "	4.50'	
E	Nozzle	6.00 "	4.00'	
F	Manway	20.00 "	4.50'	
G	Nozzle	6.00 "	3.50'	
H	Nozzle	6.00 "	4.00'	
I	Nozzle	6.00 "	4.50'	
J	Nozzle	6.00 "	5.00'	
K				
L				

Estimate Radius from Center

Roof plate thickness readings

Measure thickness every 10 feet.

Quadrant	Center	10'	20'	30'	40'	50'	60'	70'	80'	90'	Shell
North	0.248	0.249									
South											
East											
West											

Quadrant											
North											
South											
East											
West											

Minimum Thickness written in **Blue Font**

1. Tank Bottom

- Annular Ring Water Washed Blasted Product Residue Dirt/Debris
 Heavy Rust Scale Standing Water Heavy Product (Not Inspected)

2. Undesirable Bottom Conditions

See Layout and X,Y Sheet for locations

- Lap Seam Corrosion Cornerweld Corrosion Weld Pinholes Weld Cracks
 Gouges Inactive Corrosion Active Corrosion Welds Not Inspected
 Isolated Pitting Areas of Pitting Hole(s)

Topside Thresholds: Inner Plates: 0.050" Sketch Plates: 0.050" Critical Zone: 0.040"

Deepest Pitting found: None Plate Number: General Pitting:

There were no topside pits detected below the thresholds. A 20-year inspection interval was used.

3. Coating Conditions

None Thin Thick

Coating Thickness mils Peeling Cracking Holidays Blistered
 # Areas Removed Needs Further Testing Needs Repair Needs Replacement

4. Inspection Methods

See Layout and X,Y Sheet for locations

- Ultrasonic Edge Scrubs Thickness Range: 0.230-0.260" Thinnest Area Found:
 MFL 99 % of Bottom Isolated Corrosion Areas of Corrosion

Soilside Thresholds: Inner Plates: 0.200" Sketch Plates: 0.200" Critical Zone: 0.210"

Thinnest Area Found: 0.220" Plate Number: 1 General Loss:

- Vacuum Box Lap Seams Pad Plates Patch Plates Leaks Found
 MT/PT Cornerweld Lap Seams Pad Plates Patch Plates Cracks Found

There were no areas of soilside corrosion below the thresholds. A 20-year inspection interval was used.

5. Sump

(thicknesses on UES Sump form)

Quantity: 1

- Hole Corrosion Coated Water/Product Patched Not Inspected

6. Settlement

Measure on Survey Page

- Humps Sags Edge Settlement >3/8" Per Foot Needs Evaluation

A settlement survey was not performed.

STI-INTERNAL



Company: AGP

Location: Hastings, NE

Job ID: 652131

Date: 7/14/2021

Tank: DVOP 11

MinThickness 0.257

Max Thickness 0.260

AVG Thickness 0.259

Enter plate thicknesses

Plate	t	Plate	t	Plate	t	Plate	t	Plate	t
1	0.260	41		81		121		161	
2	0.257	42		82		122		162	
3		43		83		123		163	
4		44		84		124		164	
5		45		85		125		165	
6		46		86		126		166	
7		47		87		127		167	
8		48		88		128		168	
9		49		89		129		169	
10		50		90		130		170	
11		51		91		131		171	
12		52		92		132		172	
13		53		93		133		173	
14		54		94		134		174	
15		55		95		135		175	
16		56		96		136		176	
17		57		97		137		177	
18		58		98		138		178	
19		59		99		139		179	
20		60		100		140		180	
21		61		101		141		181	
22		62		102		142		182	
23		63		103		143		183	
24		64		104		144		184	
25		65		105		145		185	
26		66		106		146		186	
27		67		107		147		187	
28		68		108		148		188	
29		69		109		149		189	
30		70		110		150		190	
31		71		111		151		191	
32		72		112		152		192	
33		73		113		153		193	
34		74		114		154		194	
35		75		115		155		195	
36		76		116		156		196	
37		77		117		157		197	
38		78		118		158		198	
39		79		119		159		199	
40		80		120		160		200	



Company: AGP
 Location: Hastings, NE

Job ID: 652131
 Date: 7/14/2021
 Tank: DVOP 11

A total of _____ areas of Topsiside pitting were found. _____ of those were below thresholds.

A total of _____ areas of Soilside corrosion were found. _____ of those were below thresholds.

Min RWT 0.250

Max Pit Depth 0.000

Enter topside and soilside indications (Type S=Soilside, T=Topside, B=Both Soilside and Topside, G=Gouge, D=Dent, H=Hole)

Plate	Type	Topside Depth	Soilside RWT	Critical Zone	X	Y	Ref Corner	Comments
								No indications were found below the thresholds
<p>Note: All soilside repair plates are 12 by 12 inches unless otherwise noted. Isolated Topside pits can be puddle welded or patched.</p>								TS = Tombstone shaped

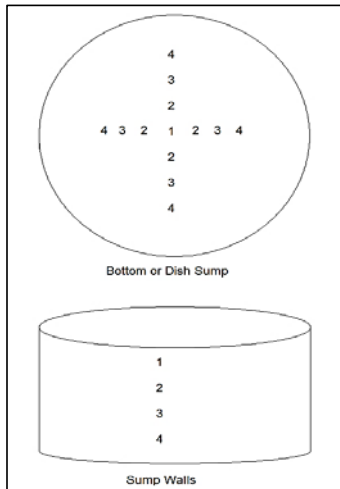
UES Thickness Scrubs

MinThickness 0.220 Max Thickness 0.260

Enter Ultrasonic Edge Scrub thicknesses (UES) 12"x12" at each station

Station	Min	Max	Station	Min	Max	Station	Min	Max
1	0.250	0.260	11			21		
2	0.220	0.260	12			22		
3	0.240	0.260	13			23		
4	0.250	0.260	14			24		
5	0.250	0.260	15			25		
6	0.250	0.260	16			26		
7	0.250	0.260	17			27		
8	0.250	0.260	18			28		
9			19			29		
10			20			30		

Sump Inspection Size: 36"x12"



	Center	North	South	East	West
1	0.256				
2		0.264	0.265	0.259	0.261
3		0.258	0.260	0.261	0.259
4		0.265	0.262	0.262	0.260


Bottom or Dish Sump

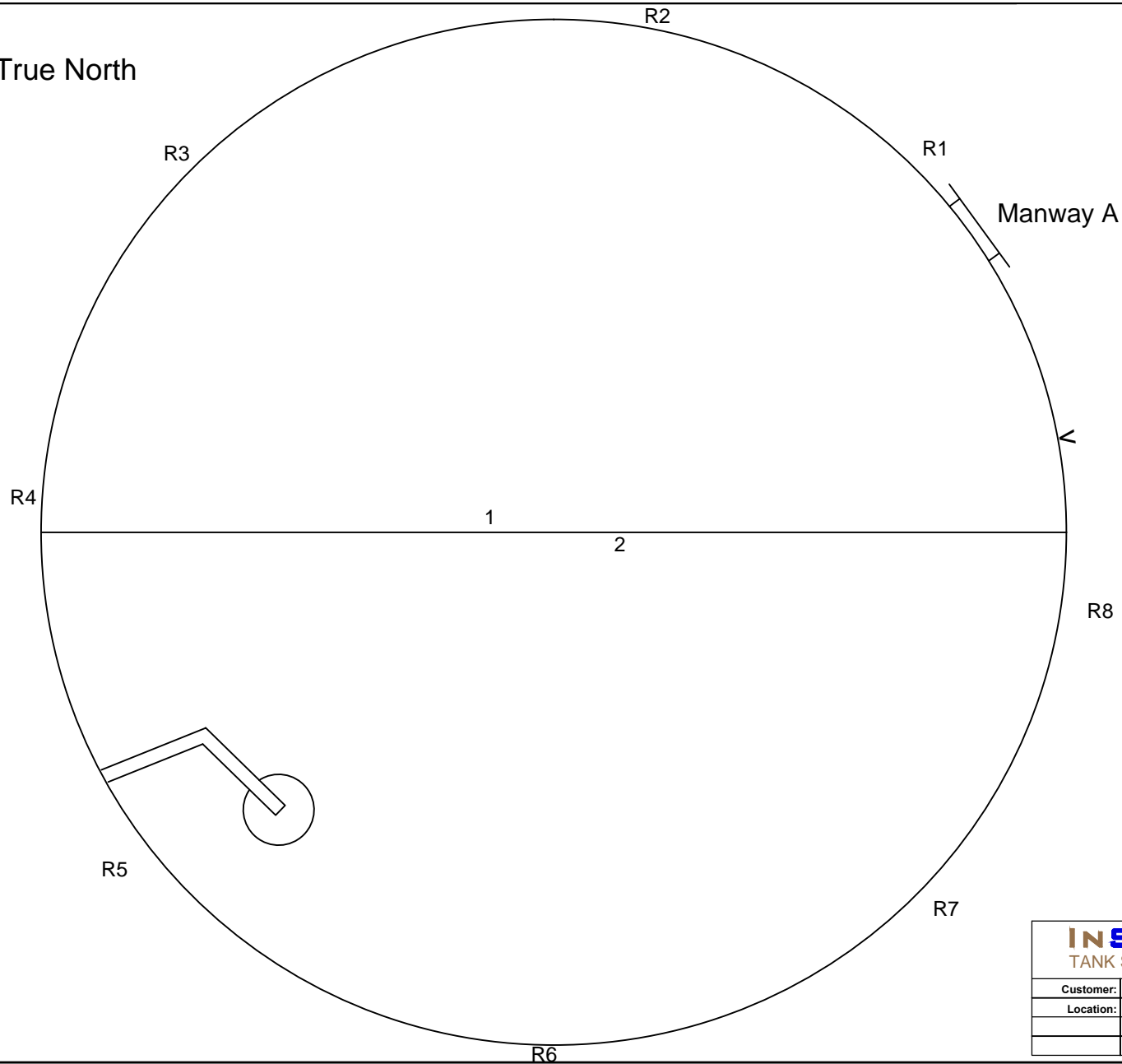
	North	South	East	West
1	0.262	0.262	0.260	0.256
2	0.254	0.262	0.260	0.259
3	0.259	0.259	0.257	0.259
4	0.257	0.259	0.259	0.256


Sump side walls



True North

- R# - Radial
-  - Sump
- > - Vertical Weld



		Job No:	652131
		Date:	07-14-2021
Customer:		AGP	
Location:		Hastings, NE	
	Diameter:	12.00	Height: 42.00
	Drawn by:	J. Bachman	Rev:

Summary

The tank was located inside a building. The open vent was not vented outside the building. The open vent extended to the lower level of the tank.

The tank had an 8-inch open vent. **A UL tank of this size would require a 10-inch emergency pressure vent per UL 142, Table 8.1.**

The coating on the external shell and appurtenances was in good condition. **This should be monitored at future inspections.**

The repads of Shell Items C, L, and M did not have telltale holes. **Consideration should be given to drilling and tapping telltale holes in the repads, pressure testing the neck and repad welds.**

The weld spacing of Shell Items C and G did not meet API standards. **Since the tank shell is 0.5 inches or less in thickness, no corrective action is required.**

Shell Items A, H, I, and J were over 2 inches in diameter and did not have repads. **Since the shell thickness is over twice the required thickness no action is required.**

There was product residue on the internal shell.

The coating on the external roof and appurtenances was in good condition. **This should be monitored at future inspections.**

A visual inspection was performed on the tank bottom to locate topside pits 0.050 inches deep and deeper in the bottom plates and 0.040 inches deep and deeper in the critical zone (within three inches of the shell) for a 20-year inspection interval. There were no pits detected below the thresholds. **No action is required.**

A Magnetic Flux Leakage (MFL) scan was performed on approximately 99 percent of the tank bottom at a remaining wall threshold of 0.200 inches thick in the bottom plates and 0.210 inches thick in the critical zone (within three inches of the shell) for a 20-year inspection interval. There were no areas of soildside corrosion below the thresholds. The lowest readings were 0.210 inches and located on Bottom Plate 1. No action is required.

Ultrasonic Edge Scrubs (UES) were performed around the entire circumference of the tank. The thicknesses ranged from 0.220 to 0.260 inches. No corrosion below the threshold were found.

The flat-bottom sump was 36 inches in diameter and 12 inches deep. The thicknesses ranged from 0.256 to 0.265 inches in the bottom of the sump and from 0.254 to 0.262 inches in the side wall. No corrosion was detected. There was product residue in the bottom of the sump.

An ultrasonic thickness reading was taken at random on each bottom plate. The thickness readings were 0.257 and 0.260 inches.

A settlement survey was not performed.

Inserv utilizes certified inspectors (STI and API-653) to perform small tank inspections in compliance with industry standards such as SP001 and API-653. The tank was categorized and inspection intervals determined per STI's SP001, 5th Edition, Table 5.5.

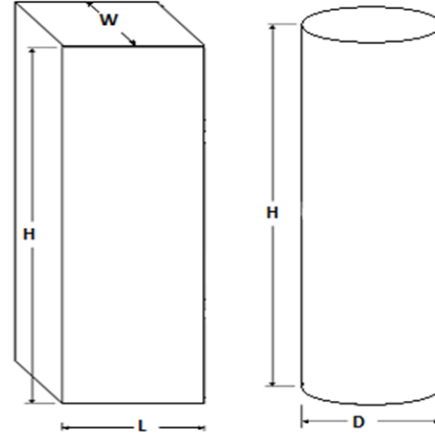
Tank DVOP 11 had a capacity of 35,291 gallons, a containment area and a CRDM (RPB, concrete pad), making it a Category 1 tank. The tank still requires periodic inspections by the owner's inspector per SP001. **The next inspection required by is an internal inspection due in 2041.**

Vertical Tank Thickness and Venting

(Not under pressure, Hydraulic head pressure only)

Inputs:

No	Rectangular Tank?	
No	Elevated Tank	
No	Stainless Steel Tank	
42.00	(ft) H	Tank Height
12.00	(ft) D	Tank Diameter 5.98 (ft) Ri Inside radius
0.70	E	Joint efficiency (use 1 for butt weld, 0.70 for lap welds)
23600	S	Allowable stress (Use 23600 if unknown steel)
62.4	lb/cf	Density of product (use 62.4 for water if unknown)
42	(ft) Hp	Height of product when full (inside tank shell)
0.244	(in) Tsm	Measured minimum thickness on shell
0.248	(in) Trm	Measured minimum thickness on roof
0.155		



Tank Properties

35292.70	Gal	Tank Capacity
1130.97	sq ft	Wetted area per UL-142
18.20	P	Internal Hydraulic Pressure (P= H(lbs/cf)/144)

Shell Circumferential Stress (longitudinal Joint) Note:1

0.167	(in) Tsl	Required thickness = $12 \cdot P \cdot Ri / (S \cdot E - 0.6 \cdot P)$ or 0.167 inches min per UL-142
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Shell Longitudinal Stress (Circumferential Joint) Note: 1

0.167	(in) Tsc	Required thickness = $12 \cdot P \cdot Ri / (S \cdot E - 0.4 \cdot P)$ or 0.167 inches min per UL-142
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Required Venting

4.00	(in)	Minimum Normal Vent per UL142 Table 8.2 Note:3
10.00	(in)	Minimum Emergency Vent per UL142 Table 8.1 Note:4

Shell Thickness evaluation per STI-SP001 4th Ed. Section10

0.167	(in) Tsr	Required shell thickness Maximum of Tsl and Tsc
0.244	(in) Tsm	Measured thickness

Shell Thickness is Okay all Categories

Shell Thickness is Okay Category 1

Shell Thickness is Okay Category 1

0.1253	75% of required thickness
0.0835	50% of required thickness
0.0418	25% of required thickness

Roof Thickness evaluation per STI-SP001 4th Ed. Section10

0.123	(in) Trr	Required roof thickness
0.248	(in) Trm	Measured roof thickness

Roof Thickness is Okay all Categories

Roof Thickness is Okay Category 1

Roof Thickness is Okay Category 1

0.0923	75% of required thickness
0.0615	50% of required thickness
0.0308	25% of required thickness

Note: 1 ASME Boiler and Pressure Vessel Code Division I, Section 8 (1986)

Note: 2 STI SP001 4th edition

Note: 3 UL-142 8th edition July 11, 2002 Tables 15.1, 8.1, 8.2

Bottom Corrosion Analysis

Per API 653 4th Edition April 2009 4.4.5

In the bottom corrosion analysis the following equations and variables are used.

$$O_r = \frac{\text{Min}(RT_{bc}, RT_{ip}) - MRT}{StPr + UPr} \quad StPr = \frac{T_o - RT_{ip}}{\text{Age}} \quad UPr = \frac{T_o - RT_{bc}}{\text{Age}}$$

T_o	(in)	Original nominal bottom thickness
Age	(yrs)	Age of Bottom Plates (May vary over bottom)
MRT	(in)	Minimum bottom thickness allowed after interval (per API 653 Table 4.4) 0.100 inches Bare steel or Thin coating no containment 0.050 inches Thick reinforced coating (>0.050") and no containment 0.050 inches bare steel or any coating with leak detection and containment
RT_{ip}	(in)	Remaining Thickness after repair of topside pitting.
RT_{bc}	(in)	Remaining Thickness after repair of soilside corrosion.
StP_r	(in/yr)	Maximum Topside corrosion rate after repair
UP_r	(in/yr)	Maximum Soilside corrosion rate after repair
O_r	(yrs)	Calculated inspection interval based on thresholds and repairs.

Notes:

- 1 Critical Zone is defined as bottom area within 3 inches of the shell.
- 2 MRT in the critical zone is lesser of 1/2 bottom plate thickness (not including corrosion allowance) or the 1/2 the ring 1 shell thickness.
- 3 If an Annular ring is required by design or use, it is evaluated per API 653 4.4.6.
- 4 If the bottom is coated StP_r is 0 (API RP652).
- 5 If the bottom has Cathodic Protection (CP), UP_r is 0 (API RP 651).
- 6 Patch plates are evaluated for soilside corrosion with UP_r minimum of RT_{ip} or RT_{bc} plus the thickness of the patch plate.

Bottom Corrosion Analysis

Per API 653 4th Edition April 2009 4.4.5

Calculated thresholds with no coating and no cathodic protection.

No	Does Tank have Annular ring?
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2021	(YYYY)	Year of inspection
20	(YY) O _{rd}	Inspection Interval
None	=	Coating type
No	=	Leak Detection & Containment
No	=	Cathodic Protection (CP)

	Include ?	Year Built	Nominal Thickness (T _o)	Topside Threshold (in)	Soilside Threshold (in)
Inner Plates	Yes	2000	0.250	0.050	0.200
Sketch Plates	Yes	2000	0.250	0.050	0.200
Critical zone	Yes	2000	0.250	0.040	0.210

MRT based on type coating, LD&C and Critical zone.

0.100	MRTi	Inner plate minimum allowable thickness
0.100	MRTs	Sketch plate minimum allowable thickness
0.125	MRTa	Critical Zone minimum allowable thickness

Age of Plates

21	AgeI
21	AgeS
21	AgeCZ

Actual Thresholds, Minimum Thicknesses and Repair Thresholds (inches)

Topside Inspection Values (values in inches)

	* Inspection Threshold Used	Max Pit depth Found	Repair Threshold used	Topside RWT after Repair
Inner Plates	0.050	0.010	No Repair	Rt _{pi} 0.240
Sketch Plates	0.050	0.010	No Repair	RT _{ipS} 0.240
Critical zone	0.040	0.010	No Repair	RT _{icZ} 0.240

* Inspection threshold for topside pitting should be rounded up to nearest 0.005 inches.

Soilside Inspection Values (values in inches)

	Inspection Threshold Used	Min Thickness Found	Repair Threshold used	Soilside RWT after Repair
Inner Plates	0.200	0.220	No Repair	Rt _{bci} 0.220
Sketch Plates	0.200	0.210	No Repair	RT _{bcs} 0.210
Critical zone	0.210	0.220	No Repair	RT _{bcsZ} 0.220

Repair Analysis for full inspection interval

	Patch Plate thickness	Top side Corr. Rate (StP _r)	Soilside Corr. Rate (UP _r)	Calculated Interval O _r (years)
Inner Plates	0.250 OK	0.0005	0.0014	20.00
Sketch Plates	0.250 OK	0.0005	0.0019	20.00
Critical zone	0.250 OK	0.0005	0.0014	20.00

Next Internal inspection due in 2041



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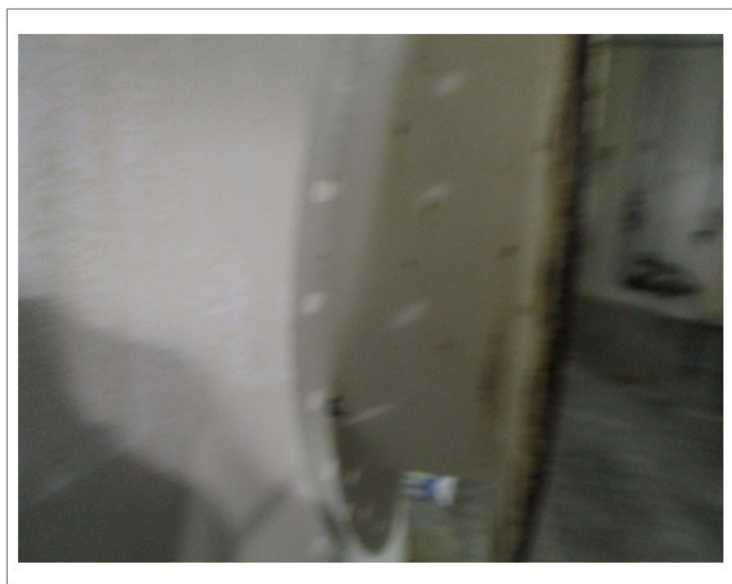
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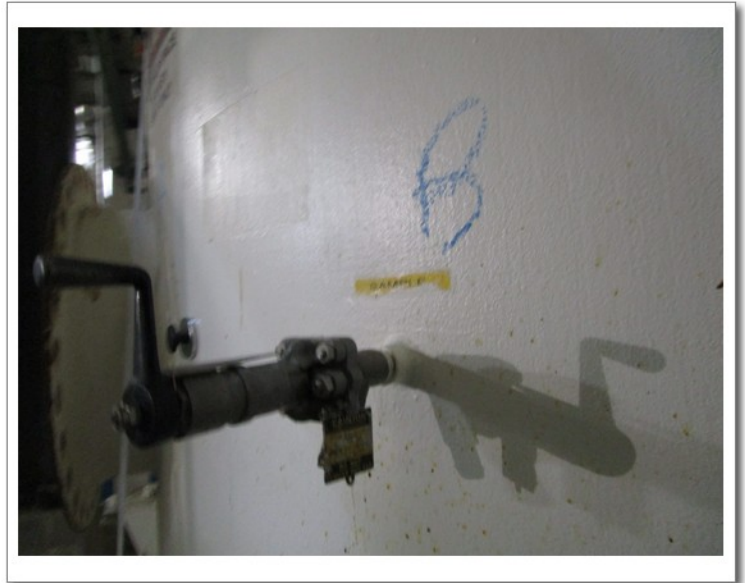
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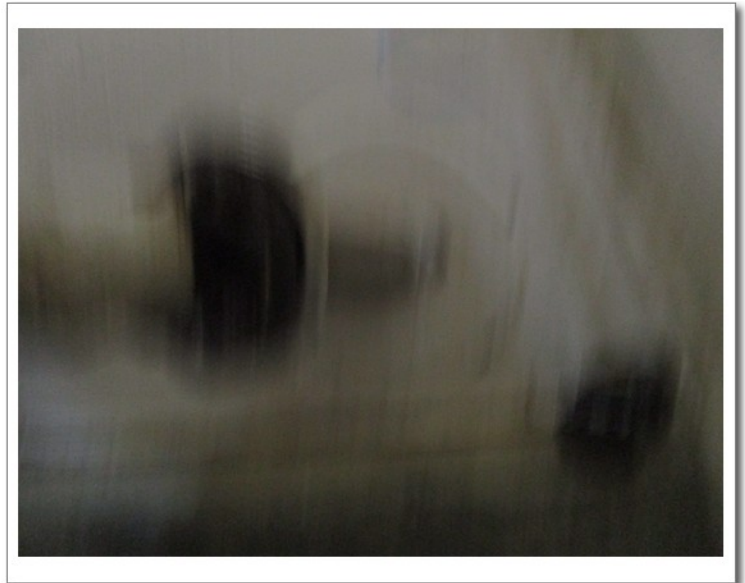
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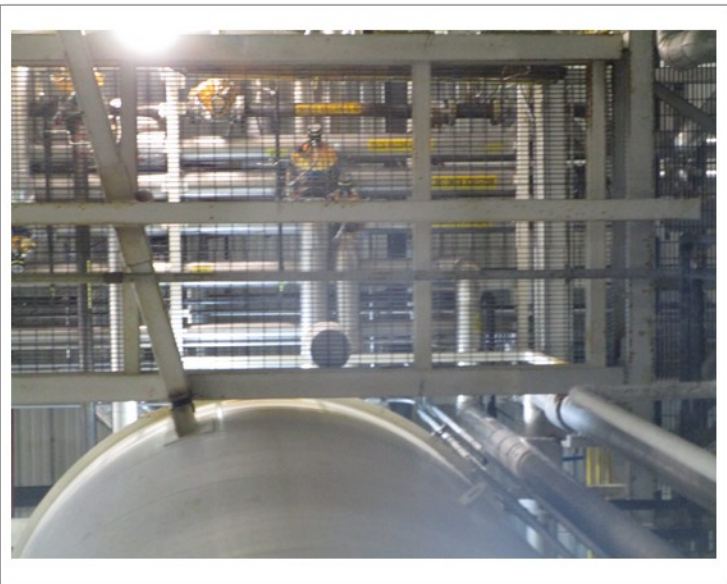
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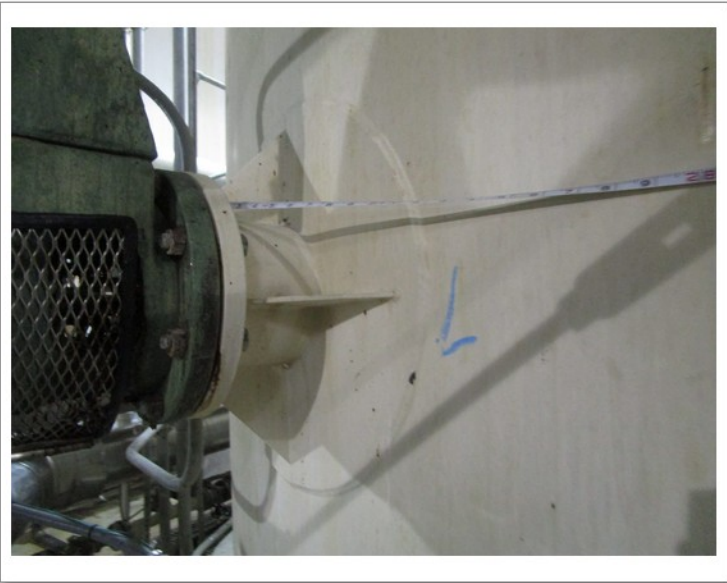
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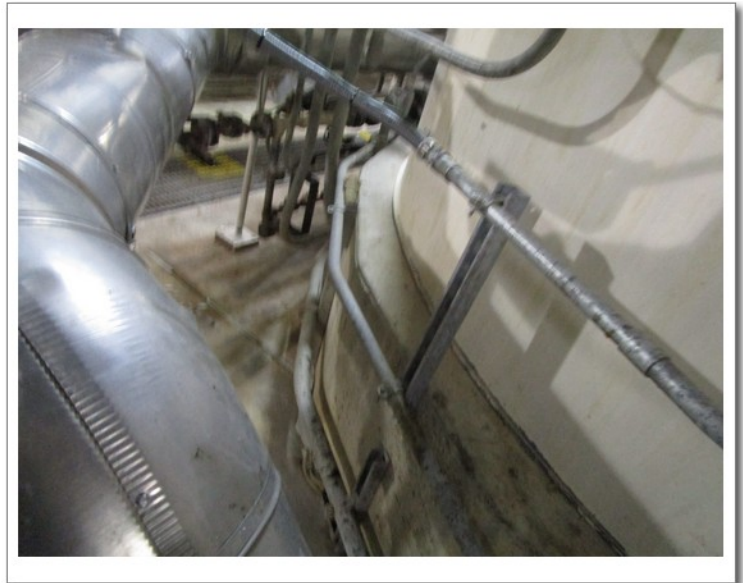
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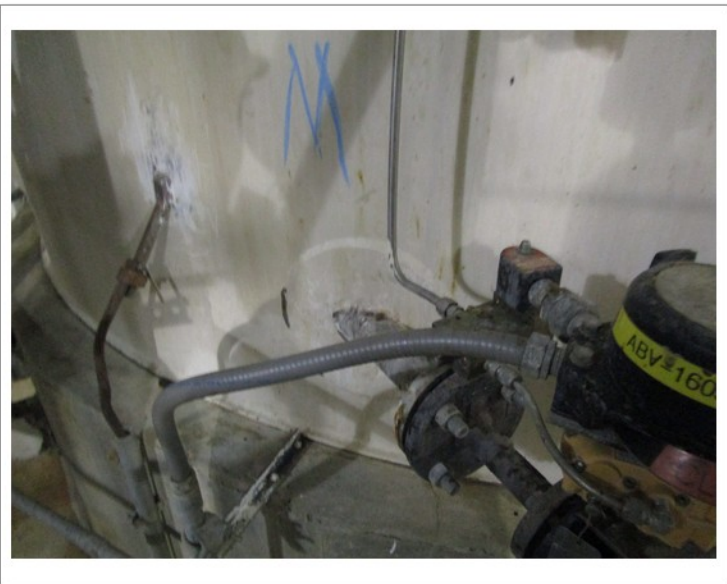
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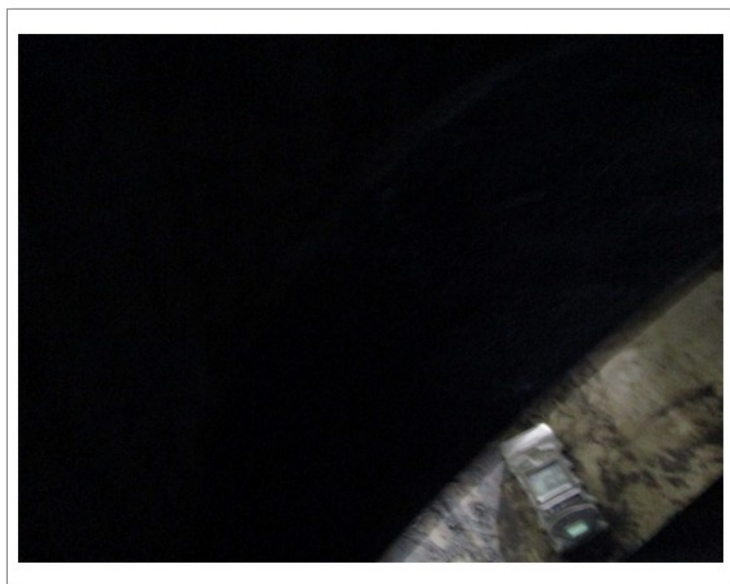
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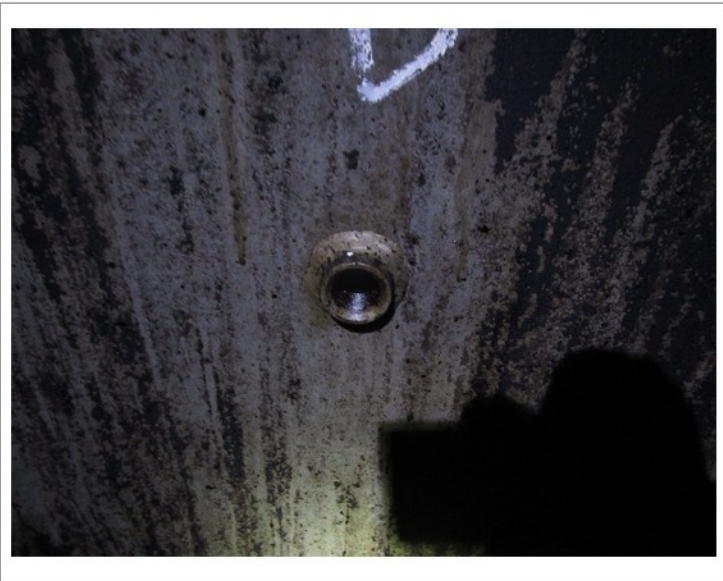
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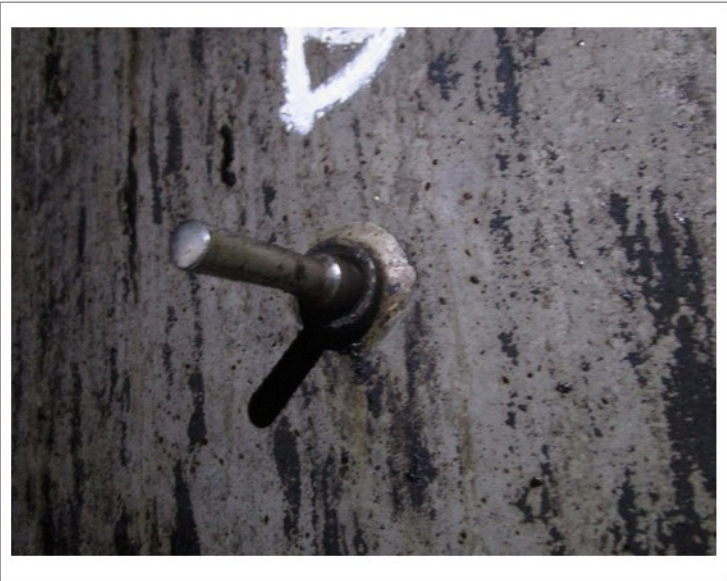
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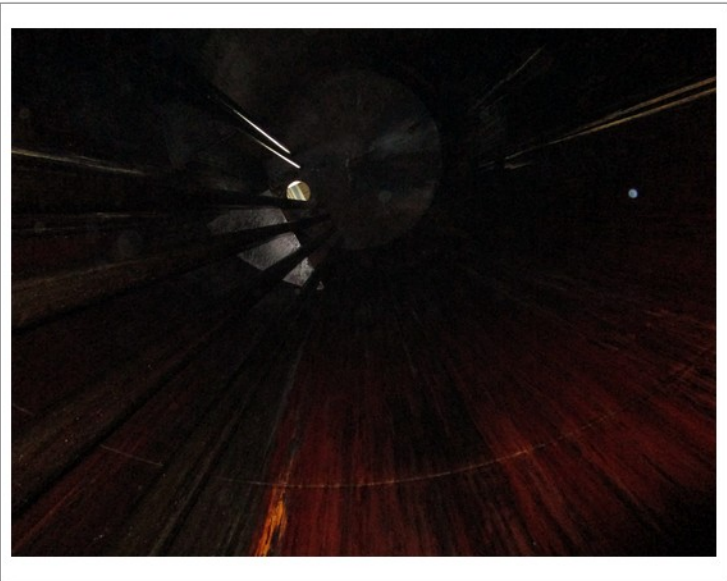
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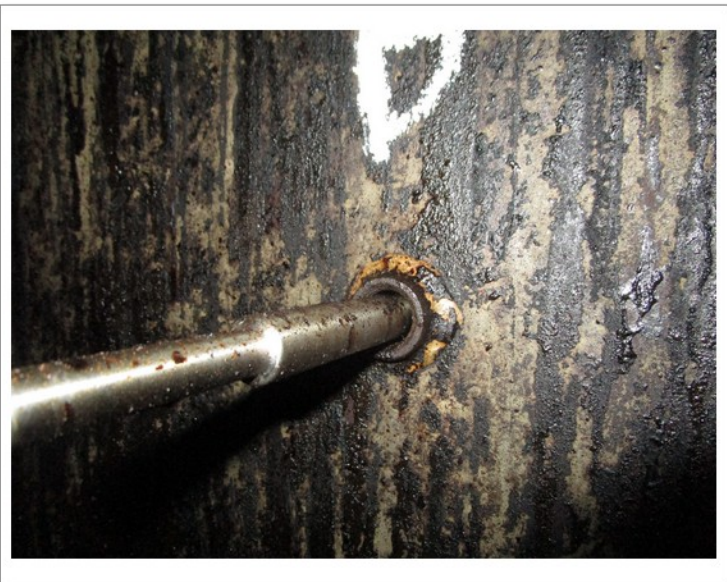
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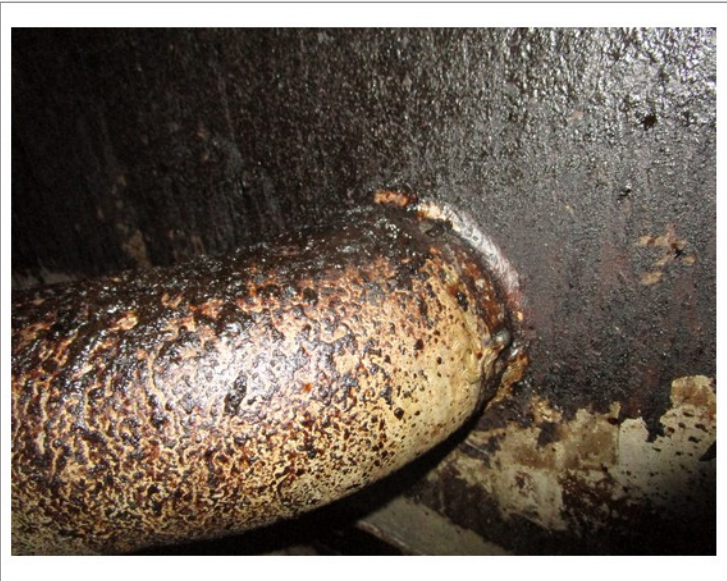
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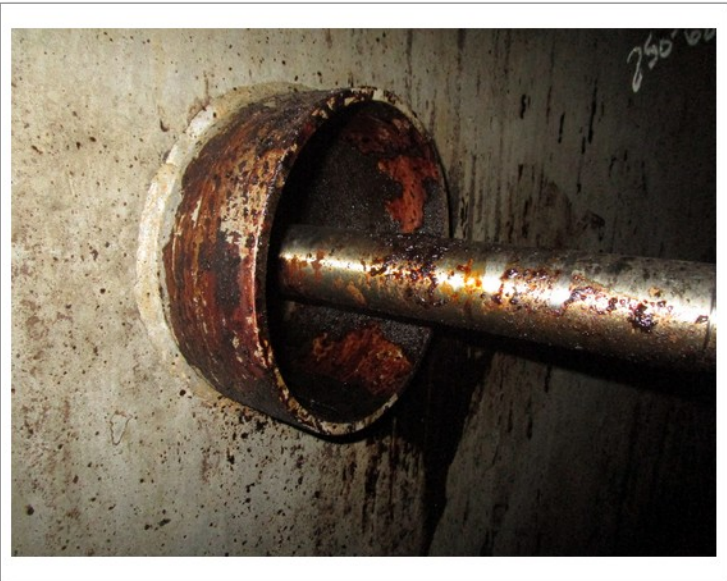
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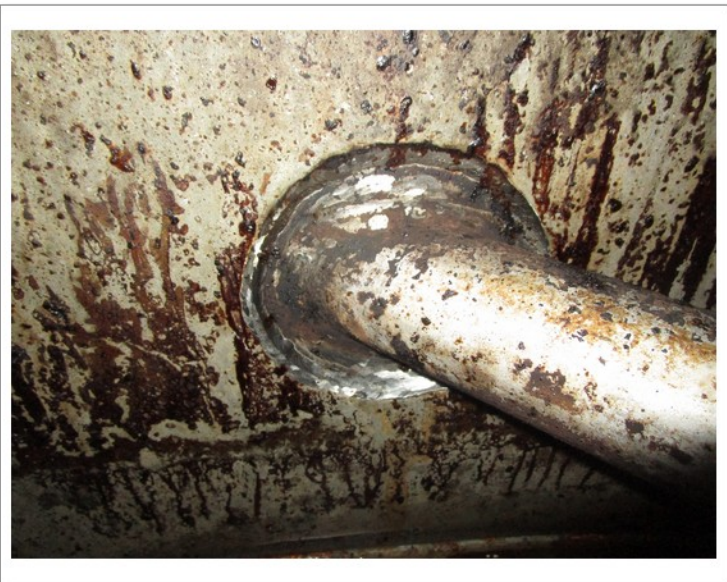
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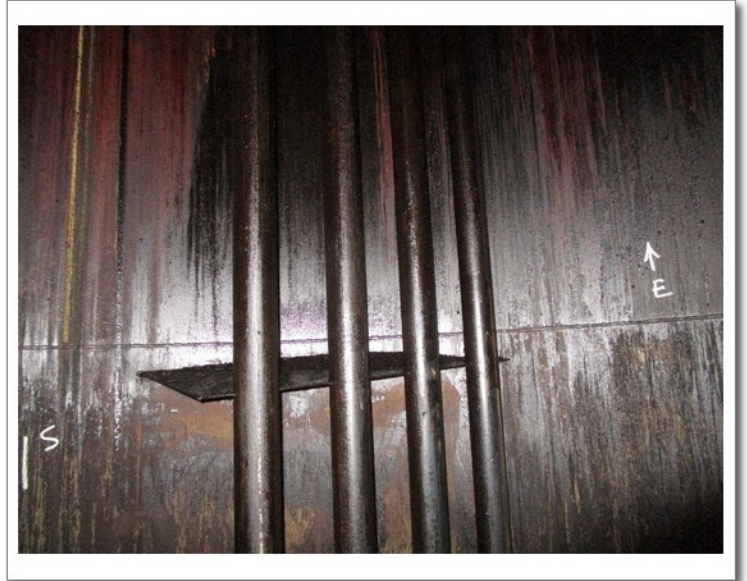
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Dear Mr. Martin:

Congratulations on passing STI SP001 Adjunct online certification course. Below is your STI Inspector identification card and certificate. We suggest that you print this page and:

- Cut out and laminate the ID card
- Frame the certificate

If you have any questions about this or any field related inspection, please feel free to call Joseph Mentzer, STI Project Engineer, at (224) 286-6469.

 **STI/SPFA**
Aboveground Tank Inspector
Certification Program
847/438-8265

Issue Date:
08/23/2019

Name: **James Martin**
STI Inspector No: **AC 44355**
Expires: **August 23, 2024**

The person to whom this card has been issued has met the requirements to attain the STI SP001 Adjunct Certification for API 653 Inspectors.
This certificate is dependent on an active API 653 certification.

CERTIFICATION

Steel Tank Institute

James Martin

STI Inspector No: **AC 44355**
Expires: **August 23, 2024**

The person whose name appears on this certificate has met all of the requirements to attain the STI SP001 Adjunct Certification for API 653 Inspectors.
This certification is dependent on an active API 653 certification.



Joseph Mentzer, P.E.
Steel Tank Institute



Issue Date:
08/23/2019

The official status of this certificate can be verified at www.steeltank.com.

API Individual Certification Programs

verifies that

James William Martin

has met the requirements for API certification

*API-653 Aboveground Storage Tank
Inspector*

Certification Number *32455*

Original Certification Date *April 30, 2008*

Current Certification Date *April 30, 2020*

Expiration Date *April 30, 2023*



Manager, Individual Certification Programs

ULTRASONIC TESTING

THIS ACKNOWLEDGES THAT

James Martin

HAS SUCCESSFULLY COMPLETED THE REQUIREMENTS OF INSERV INSPECTION AND CONSULTING SERVICES LLC
QUALIFICATION AND CERTIFICATION OF NDE PERSONNEL WRITTEN PRACTICE REFERENCING ASNT-TC-1A

LEVEL II

**DECEMBER
9TH 2020**

x

SIGNED, *James Martin*
Authorized NDT Level III

INSERV

INTEGRATED SERVICE COMPANY LLC